

***Field Data Printouts***

Project Number	3648
Client	Big Rivers
Plant	Henderson
Location	Unit 2 Inlet
Date	8/4/2011
Filter ID	M-5
Y <sub>d</sub>	0.9953
Pitot C <sub>p</sub>	0.84

Place an "x" in the appropriate Box

Nozzle Diameter (in)	0.200
Filter ID	12152
Titan Type	Impinger
Titan ID	IB-23
P <sub>h</sub> (Inches Hg)	29.41
P <sub>s</sub> (Inches H <sub>2</sub> O)	-6.0
Start Time	7:19
Stop Time	9:15

Circular?	
Peculiar?	x
Diameter	
Length	186
Width	139

Moisture	Final Wt (g)	Tare Wt (g)	Net Wt (g)
Impinger 1	767.5	595.5	172.0
Impinger 2	690.3	739.7	-49.4
Impinger 3	571.8	567.5	4.3
Silica Gel	913.3	897.7	15.6
Weight of Water Collected, W <sub>w</sub> (g)			126.9
Silica Gel Net Weight, W <sub>sg</sub> (g)			15.6

CEMS	%CO <sub>2</sub>	%CO <sub>2</sub> +%O <sub>2</sub>	%O <sub>2</sub>
Average	13.3	N/A	5.62

Run 1

Traverse Point	4	Velocity Pressure ΔP (in H <sub>2</sub> O)	Orifice Setting ΔH (in H <sub>2</sub> O)	Gas Sample Volume Initial (ft <sup>3</sup> )	Stack Temp (°F)	DGM Inlet (°F)	DGM Outlet (°F)	Square Root ΔP	Stack Gas Velocity vs (ft/sec)	Volume Metered (ft <sup>3</sup> )	Isokinetic (%)
	Elapsed Time										
				898.20							
1-1	4.0	0.72	0.86	900.24	316	84	81	0.849	58.6	1.346	102.8
1-2	8.0	0.75	0.90	902.14	317	85	82	0.866	59.8	1.309	92.4
1-3	12.0	0.75	0.90	904.22	318	85	82	0.866	59.9	1.981	106.3
1-4	16.0	0.75	0.90	906.25	316	86	82	0.966	58.3	1.931	105.5
1-5	20.0	0.88	0.82	908.20	316	86	82	0.825	56.9	1.956	106.4
2-1	24.0	1.00	1.20	909.93	317	86	83	1.000	68.1	1.645	77.4
2-2	28.0	1.00	1.20	913.00	318	86	84	1.000	69.1	2.917	138.2
2-3	32.0	1.00	1.20	914.45	318	87	85	1.000	69.1	1.375	65.1
2-4	36.0	1.00	1.20	917.90	318	88	85	1.000	69.1	3.269	154.8
2-5	40.0	0.85	1.00	920.12	318	89	85	0.922	63.7	2.101	107.9
3-1	44.0	1.10	1.30	922.32	316	90	86	1.045	72.4	2.080	95.6
3-2	48.0	1.00	1.20	924.70	316	91	87	1.000	69.1	2.245	106.2
3-3	52.0	1.10	1.30	927.06	316	91	88	1.045	72.4	2.225	100.3
3-4	56.0	1.10	1.30	929.50	316	92	88	1.049	72.4	2.284	103.8
3-5	60.0	1.20	1.40	932.01	316	93	88	1.095	75.6	2.383	102.0
4-1	64.0	1.20	1.40	934.52	314	94	89	1.095	75.5	2.358	101.7
4-2	68.0	1.30	1.60	937.20	314	95	90	1.140	78.0	2.515	108.2
4-3	72.0	1.20	1.40	939.72	314	96	91	1.095	75.5	2.359	101.7
4-4	76.0	1.10	1.30	942.20	314	97	92	1.049	72.3	2.517	104.4
4-5	80.0	1.10	1.30	944.63	314	98	92	1.049	72.3	2.668	102.2
5-1	84.0	0.65	0.78	946.62	314	99	94	0.805	55.6	1.950	108.4
5-2	88.0	0.70	0.84	948.60	314	99	94	0.837	57.7	1.841	103.9
5-3	92.0	0.75	0.90	950.89	314	99	94	0.866	59.7	2.130	116.2
5-4	96.0	0.75	0.90	952.70	314	99	94	0.866	58.7	1.653	91.9
5-5	100	0.80	0.96	954.83	314	99	94	0.894	61.7	1.981	104.6

Totals and Averages											
	100		1.12	56.63	316		89.7	0.965	66.6	53.34	104.5

Project Number	3648
Client	Big Rivers
Plant	Henderson
Location	Unit 2 Inlet
Date	8/4/2011
Meter ID	M-5
Y <sub>2</sub>	0.9953
Filter C <sub>2</sub>	0.84

Place an "x" in the appropriate Box

Nozzle Diameter (in)	0.200
Filter ID	12153
Train Type	Impinger
Train ID	IB-A
F <sub>b</sub> (Inches Hg)	29.41
F <sub>s</sub> (Inches H <sub>2</sub> O)	-6.0
Start Time	10:09
Stop Time	12:00

Circular?	
Rectangular?	x
Diameter	
Length	186
Width	139

Moisture	Final Wt (g)	Tare Wt (g)	Net Wt (g)
Impinger 1	667.7	560.2	107.5
Impinger 2	727.2	733.2	-6.0
Impinger 3	641.2	628.7	12.5
Silica Gel	885.5	874.2	11.3
Weight of Water Collected (g)			113.0
Silica Gel Net Weight, V <sub>W,2</sub> (g)			11.3

CEMS	%CO <sub>2</sub>	%CO <sub>2</sub> +%O <sub>2</sub>	%O <sub>2</sub>
Average	13.2	NA	5.60

Run 2

Train/Train Point	Min/Plt	Velocity Pressure in F (in H <sub>2</sub> O)	Orifice Setting A/H (in H <sub>2</sub> O)	Gas Sample Volume Initial (ft <sup>3</sup> )	Stack Temp (°F)	DGM Inlet (°F)	DGM Outlet (°F)	Square Root P	Stack Gas Velocity V <sub>s</sub> (ft/sec)	Volume Measured (ft <sup>3</sup> )	Isokinetic (%)
	4 Elapsed Time										
				974.60							
1-1	4.0	1.00	1.20	977.00	318	105	100	1.000	69.0	2.210	105.8
1-2	8.0	1.00	1.20	979.32	318	105	100	1.000	69.0	2.198	100.4
1-3	12.0	1.00	1.20	981.57	318	105	100	1.000	69.0	2.072	97.3
1-4	16.0	1.00	1.20	983.97	318	106	100	1.000	69.0	2.208	100.7
1-5	20.0	0.83	1.00	986.20	318	107	100	0.911	62.9	2.049	105.7
2-1	24.0	1.10	1.30	988.55	318	107	100	1.049	72.4	2.160	96.8
2-2	28.0	1.10	1.30	990.98	318	107	100	1.049	72.4	2.234	100.1
2-3	32.0	1.20	1.40	993.52	318	107	100	1.095	75.6	2.336	100.2
2-4	36.0	1.00	1.20	995.99	318	107	100	1.000	69.0	2.270	100.7
2-5	40.0	1.10	1.30	998.37	318	108	100	1.049	72.4	2.136	97.9
3-1	44.0	1.30	1.60	1000.00	318	108	100	1.140	78.7	1.996	61.7
3-2	48.0	1.20	1.40	1002.75	318	108	100	1.095	75.6	2.026	108.4
3-3	52.0	1.20	1.40	1005.84	318	108	100	1.095	75.6	1.839	121.8
3-4	56.0	1.20	1.40	1008.30	318	108	100	1.095	75.6	2.260	96.5
3-5	60.0	1.10	1.30	1010.63	318	108	100	1.049	72.4	2.140	95.8
4-1	64.0	0.72	0.86	1012.62	318	107	100	0.845	58.6	1.827	101.2
4-2	68.0	0.89	0.83	1014.52	318	106	100	0.831	57.0	1.746	98.9
4-3	72.0	0.80	0.96	1016.58	318	106	100	0.955	61.7	1.594	95.5
4-4	76.0	0.86	1.00	1018.67	318	106	100	0.822	63.6	1.922	97.9
4-5	80.0	0.66	0.78	1020.51	318	106	100	0.805	55.7	1.681	98.5
5-1	84.0	0.72	0.86	1022.47	318	105	100	0.845	58.6	1.803	98.9
5-2	88.0	0.75	0.90	1024.44	318	105	100	0.938	65.5	1.812	98.3
5-3	92.0	0.75	0.90	1026.45	318	105	100	0.866	59.8	1.949	100.3
5-4	96.0	0.75	0.90	1028.37	318	105	100	0.965	69.8	1.766	95.8
5-5	100	0.68	0.82	1,030.31	318	105	100	0.825	56.9	1.785	101.7

Totals and Averages											
	100		1.13	55.71	318	105		0.968	66.8	51.22	99.4

Project Number	3648
Client	Big Rivers
Plant	Henderson
Location	Unit 2 Inlet
Date	8/4/2011
Meier ID	M-5
Y <sub>c</sub>	0.9953
Pitot C <sub>p</sub>	0.84

Place an "x" in the appropriate Box

Nozzle Diameter (in)	0.200
Filter ID	12154
Titan Type	Impinger
Titan ID	IB-25
P <sub>3</sub> (Inches Hg)	29.41
P <sub>4</sub> (Inches H <sub>2</sub> O)	-5.5
Start Time	13:11
Stop Time	15:02

Circular?	
Rectangular?	x
Diameter	
Length	186
Width	139

Moisure	Final Wt (g)	Tare Wt (g)	Net Wt (g)
Impinger 1	717.0	596.0	121.0
Impinger 2	731.0	737.0	-5.0
Impinger 3	574.5	567.9	6.6
Silica Gel	925.4	913.2	12.2
Weight of Water Collected, V <sub>w</sub> (g)			121.6
Silica Gel Net Weight, V <sub>sg</sub> (g)			12.2

CEMS	%CO <sub>2</sub>	%CO <sub>2</sub> +%O <sub>2</sub>	%O <sub>2</sub>
Average	13.3	NA	5.5

Run 3

Traverse Point	min/Pk	Velocity Pressure ΔP (in H <sub>2</sub> O)	Orifice Setting ΔH (in H <sub>2</sub> O)	Gas Sample Volume Initial (ft <sup>3</sup> )	Stack Temp (°F)	DGM Inlet (°F)	DGM Outlet (°F)	Square Foot ΔP	Stack Gas Velocity V <sub>s</sub> (ft/sec)	Volume Metered (ft <sup>3</sup> )	Kinetics (%)
	4										
1-1	4.0	1.00	1.20	34.53	319	99	95	1.000	69.2	2.073	98.2
1-2	8.0	1.10	1.30	36.79	319	99	95	1.049	72.6	2.102	95.1
1-3	12.0	1.00	1.20	37.01	319	99	95	1.000	69.2	2.065	97.7
1-4	16.0	1.00	1.20	39.24	319	99	95	1.000	69.2	2.073	98.4
1-5	20.0	0.85	1.00	41.32	319	99	95	0.922	63.8	1.932	99.6
2-1	24.0	1.10	1.30	42.85	319	100	96	1.048	72.6	1.420	64.2
2-2	28.0	1.00	1.20	45.10	319	100	97	1.000	69.2	2.086	99.0
2-3	32.0	1.00	1.20	47.28	319	101	99	1.000	69.2	2.016	95.7
2-4	36.0	1.00	1.20	49.39	319	101	99	1.000	69.2	1.951	92.6
2-5	40.0	1.20	1.40	51.92	319	102	99	1.095	75.8	2.339	101.5
3-1	44.0	1.20	1.40	54.25	319	102	98	1.095	75.8	2.156	95.3
3-2	48.0	1.20	1.40	56.68	319	102	98	1.095	75.8	2.248	97.4
3-3	52.0	1.20	1.40	59.15	320	102	99	1.095	75.8	2.293	99.0
3-4	56.0	1.20	1.40	61.49	321	102	99	1.095	75.8	2.183	93.9
3-5	60.0	1.20	1.40	63.74	321	102	99	1.095	75.8	2.080	90.2
4-1	64.0	0.75	0.90	65.73	321	102	100	0.866	60.0	1.636	100.7
4-2	68.0	0.75	0.90	67.70	321	102	100	0.866	60.0	1.817	98.7
4-3	72.0	0.81	0.97	69.80	321	102	100	0.900	62.3	1.938	102.3
4-4	76.0	0.83	1.00	71.93	321	102	100	0.911	63.1	1.365	102.5
4-5	80.0	0.81	0.97	74.00	321	102	100	0.900	62.3	1.310	100.8
5-1	84.0	0.80	0.96	76.02	321	103	100	0.894	62.0	1.862	98.9
5-2	88.0	0.80	0.96	78.13	321	103	100	0.894	62.0	1.935	103.3
5-3	92.0	0.75	0.90	80.25	321	103	100	0.866	60.0	1.954	107.2
5-4	96.0	0.75	0.90	82.38	321	103	100	0.866	60.0	1.963	107.7
5-5	100	0.77	0.92	85.30	321	103	100	0.877	60.8	2.691	145.7

Totals and Averages

100		1.14	53.00	320	99.8	0.977	67.7	49.02	95.3
-----	--	------	-------	-----	------	-------	------	-------	------

Project Number	3648
Client	Big Rivers
Plant	Henderson
Location	Unit 2 Inlet
Date	8/4/2011
Meter ID	M-20
Year	0.9952
Print	0.84

Place an "x" in the appropriate Box

Nozzle Diameter (in)	0.200
Filter ID	NA
Train Type	Impingers
Train ID	IB14
P <sub>1</sub> (Inches Hg)	29.41
P <sub>2</sub> (Inches H <sub>2</sub> O)	-5.5
Start Time	7:19
Stop Time	9:23

Circular?	
Rectangular?	x
Diameter	
Length	186
Width	139

Impinger	Final Wt (g)	Tare Wt (g)	Net Wt (g)
Impinger 1	843.5	720.0	123.5
Impinger 2	590.5	578.1	12.4
Impinger 3	631.5	622.2	9.3
Silica Gel	925.0	909.0	16.0
Weight of Water Collected, W <sub>w</sub> (g)			145.2
Silica Gel Net Weight, W <sub>sil</sub> (g)			16.0

CEMS	%CO <sub>2</sub>	%CO <sub>2</sub> +%O <sub>2</sub>	%O <sub>2</sub>
Average	12.5	NA	5.62

Run 1

Transverse Point	Min/Pt	Velocity Pressure ΔP (in H <sub>2</sub> O)	Orifice Setting ΔH (in H <sub>2</sub> O)	Gas Sample Volume Initial (ft <sup>3</sup> )	Stack Temp (°F)	DGIM Inlet (°F)	DGIM Outlet (°F)	Square Root ΔP	Stack Gas Velocity (ft/sec)	Volume Measured (ft <sup>3</sup> )
	10 Elapsed Time									
Single	10	0.90	1.00	542.30	318	90	87	0.946	65.5	5.332
	20	0.87	0.97	563.52	317	99	89	0.935	64.3	5.204
	30	0.89	0.99	559.17	317	99	89	0.943	65.1	5.279
	40	0.93	1.00	584.88	316	101	92	0.981	66.5	5.311
	50	0.90	1.00	570.56	319	102	93	0.949	65.5	5.273
	60	0.93	1.00	576.27	316	103	95	0.964	66.5	5.287
	70	0.90	1.00	581.98	316	104	95	0.949	65.4	5.263
	80	0.87	0.99	587.78	316	105	97	0.933	64.3	5.170
	90	0.90	1.00	593.40	317	107	97	0.949	65.4	5.176
	100	0.87	0.99	589.07	316	106	99	0.933	64.3	5.217
	110	0.89	0.99	604.76	315	105	98	0.943	65.0	5.245
	120	0.87	0.99	610.38	315	103	98	0.935	64.3	5.190

Totals and Averages

120	0.993	68.08	317	98.0	0.945	65.2	63.14
-----	-------	-------	-----	------	-------	------	-------

Project Number	3648
Client	Big Rivers
Plant	Henderson
Location	Unit 2 Inlet
Date	8/4/2011
Header ID	M-20
V <sub>1</sub>	0.9952
Pitot C <sub>p</sub>	0.84

Place an "x" in the appropriate Box

Nozzle Diameter (in)	0.200
Filter ID	NA
Train Type	Impingers
Train ID	IB-25
P <sub>1</sub> (Inches Hg)	29.41
P <sub>2</sub> (Inches H <sub>2</sub> O)	-5.5
Start Time	10:09
Stop Time	12:12

Circular?	
Rectangular?	x
Diameter	
Length	186
Width	139

Impinger	Final Wt (g)	Tare Wt (g)	Net Wt (g)
Impinger 1	852.0	718.7	133.3
Impinger 2	744.3	734.6	9.7
Impinger 3	640.0	634.6	5.4
Silica Gel	924.5	909.6	14.9
Weight of Water Collector V <sub>1</sub> (g)			148.4
Silica Gel Net Weight V <sub>2</sub> (g)			14.9

CEMS	%CO <sub>2</sub>	%CO <sub>2</sub> +%O <sub>2</sub>	%O <sub>2</sub>
Average	12.2	NA	3.60

Run 2

Traverse Point	Min/Pi	Velocity Pressure Δ F (in H <sub>2</sub> O)	Orifice Setting Δ H (in H <sub>2</sub> O)	Gas Sample Volume Initial (ft <sup>3</sup> )	Stack Temp. (°F)	DGM Inlet (°F)	DGM Outlet (°F)	Square Point Δ P	Stack Gas Velocity V <sub>s</sub> (ft/sec)	Volume Measured (ft <sup>3</sup> )
	10			611.89						
Single	10	0.90	1.00	617.63	317	94	92	0.949	65.5	5.372
	20	0.87	0.97	623.31	317	99	93	0.933	64.4	5.287
	30	0.88	0.98	628.94	317	102	93	0.938	64.7	5.227
	40	0.90	1.00	634.76	317	101	94	0.948	65.5	5.165
	50	0.89	0.99	640.35	317	102	94	0.943	65.1	5.185
	60	0.93	1.00	646.10	317	101	94	0.964	66.6	5.338
	70	0.90	1.00	651.73	317	100	93	0.959	65.5	5.296
	80	0.90	1.00	657.43	317	100	93	0.949	65.5	5.301
	90	0.91	1.00	663.10	317	100	93	0.954	65.8	5.274
	100	0.91	1.00	668.84	319	102	96	0.954	65.6	5.315
	110	0.92	1.00	674.68	318	103	96	0.959	66.2	5.405
	120	0.90	1.00	680.34	319	104	97	0.949	65.6	5.227

Totals and Averages

120	0.995	68.45	317	97.3	0.949	65.5	63.57
-----	-------	-------	-----	------	-------	------	-------

Project Number	3648
Client	Big Rivers
Plant	Henderson
Location	Unit 2 Inlet
Date	8/4/2011
Meter ID	M-20
Y <sub>3</sub>	0.9952
Flow Q <sub>3</sub>	0.84

Nozzle Diameter (in)	0.200
Filter ID	NA
Train Type	Impingers
Train ID	IB14
P <sub>0</sub> (Inches Hg)	29.41
P <sub>1</sub> (Inches H <sub>2</sub> O)	-5.5
Start Time	13:11
Stop Time	15:15

Place an "x" in the appropriate Box

Circular?	
Rectangular?	x
Diameter	
Length	186
Width	139

Metric	Final W <sub>i</sub> (g)	Tare W <sub>i</sub> (g)	Net W <sub>i</sub> (g)
Impinger 1	828.7	722.1	106.6
Impinger 2	609.3	578.9	30.4
Impinger 3	631.2	621.7	9.5
Silica Gel	936.5	924.0	12.5
Weight of Water Collected, V <sub>wt</sub> (g)			146.5
Silica Gel Net Weight, V <sub>wg</sub> (g)			12.5

CEMS	%CO <sub>2</sub>	%CO <sub>2</sub> +%O <sub>2</sub>	%O <sub>2</sub>
Average	13.2	NA	5.14

Run 3

Transverse Point	Min/Pl	Velocity Pressure ΔP (in H <sub>2</sub> O)	Orifice Setting ΔH (in H <sub>2</sub> O)	Gas Sample Volume Initial (ft <sup>3</sup> )	Stack Temp (°F)	DGM Inlet (°F)	DGM Outlet (°F)	Square Root ΔP	Stack Gas Velocity (ft/sec)	Volume Measured (ft <sup>3</sup> )
	Elapsed Time									
Single	10	0.91	1.00	687.52	318	104	105	0.964	66.8	5.236
	20	0.90	1.00	693.20	318	105	105	0.949	65.4	5.203
	30	0.90	1.00	698.95	318	110	107	0.949	65.4	5.235
	40	0.89	0.99	704.76	318	115	109	0.943	65.1	5.257
	50	0.90	1.00	710.50	319	118	113	0.946	65.5	5.162
	60	0.92	1.00	716.35	319	120	113	0.958	66.2	5.262
	70	0.89	0.99	722.10	318	122	116	0.943	65.1	5.140
	80	0.93	1.00	727.88	318	124	119	0.964	66.5	5.145
	90	0.90	1.00	733.67	318	124	120	0.949	65.4	5.149
	100	0.88	0.98	739.20	318	124	120	0.938	64.7	4.916
	110	0.90	1.00	748.41	319	126	121	0.949	65.5	5.170
	120	0.91	1.00	754.73	318	124	121	0.954	65.9	5.616

Totals and Averages

120	0.997	72.92	318	118	0.950	65.5	65.52
-----	-------	-------	-----	-----	-------	------	-------

Project Number	3648
Client	Big Rivers
Plant	Henderson
Location	Inlet
Date	8/4/2011
Meter ID	M-14
Yd	1.0087
Pilot C <sub>2</sub>	0.84

Place an "x" in the appropriate Box

Nozzle Diameter (in)	0.195
Filter ID	NA
Train Type	Impinger
Train ID	NEW
P <sub>1</sub> (Inches Hg)	29.41
P <sub>2</sub> (Inches H <sub>2</sub> O)	-6.0
Start Time	7:19
Stop Time	9:35

Circular?	
Rectangular?	x
Diameter	
Length	186
Width	139

Moisture	Final Wt (g)	Tare Wt (g)	Net Wt (g)
Impinger 1	847.6	519.9	127.7
Impinger 2	623.6	609.1	14.5
Impinger 3	720.5	711.6	8.9
Impinger 4	622.9	619.1	3.8
Silica Gel	919.7	900.8	18.9
Weight of Water Collected, W <sub>w</sub> (g)			154.9
Silica Gel Net Weight, W <sub>sg</sub> (g)			16.8

CEMS	%CO <sub>2</sub>	%CO <sub>2</sub> +%O <sub>2</sub>	%O <sub>2</sub>
Average	13.2	NA	6.62

Run 1

Traverse Point #	5		Velocity Pressure ΔP (in H <sub>2</sub> O)	Orifice Setting ΔH (in H <sub>2</sub> O)	Gas Sample Volume Initial (ft <sup>3</sup> )	Stack Temp (°F)	DGM Inlet (°F)	DGM Outlet (°F)	Square Root ΔP	Stack Gas Velocity vs (ft/sec)	Volume Measured (ft <sup>3</sup> )	Isokinetics (%)
	min	sec										
1-1	5	0.65	0.67	835.76	316	87	86	0.806	55.7	2.168	107.2	
1-2	10	0.72	0.73	838.11	316	88	83	0.849	58.6	2.259	106.1	
1-3	15	0.80	0.82	840.48	319	90	85	0.894	61.9	2.270	107.3	
1-4	20	0.87	0.89	843.09	325	93	85	0.933	64.6	2.492	107.2	
1-5	25	0.83	0.64	845.30	326	95	86	0.794	55.2	2.104	106.3	
2-1	30	0.80	0.82	847.89	313	95	87	0.894	61.7	2.168	109.2	
2-2	35	0.83	0.85	850.46	313	95	88	0.911	62.8	2.144	106.7	
2-3	40	1.10	1.10	853.31	317	98	89	1.049	72.5	2.702	102.7	
2-4	45	1.20	1.20	856.29	325	100	90	1.095	76.1	2.818	103.1	
2-5	50	0.93	0.95	859.05	326	101	90	0.984	67.0	2.606	108.4	
3-1	55	0.95	0.97	861.78	316	100	93	0.875	67.3	2.573	105.2	
3-2	60	0.97	0.99	864.58	317	100	93	0.985	68.1	2.640	106.9	
3-3	65	1.00	1.00	867.37	322	103	95	1.000	69.3	2.618	104.8	
3-4	70	1.00	1.00	870.15	325	104	95	1.000	69.5	2.607	104.5	
3-5	75	0.85	0.87	872.81	325	105	96	0.922	64.1	2.489	105.2	
4-1	80	1.00	1.00	875.65	314	104	97	1.000	69.0	2.658	105.8	
4-2	85	1.10	1.10	878.50	316	105	97	1.049	72.3	2.636	101.5	
4-3	90	1.20	1.20	881.50	320	107	98	1.095	75.9	2.799	102.1	
4-4	95	1.10	1.10	884.39	320	107	98	1.049	72.6	2.696	102.7	
4-5	100	0.91	0.93	887.22	320	108	99	0.954	66.1	2.614	110.2	
5-1	105	1.10	1.10	889.93	320	108	99	1.049	72.6	2.524	96.2	
5-2	110	1.30	1.30	892.64	321	108	99	1.140	75.0	2.325	80.5	
5-3	115	1.10	1.10	895.40	320	108	99	1.049	72.6	2.654	101.1	
5-4	120	1.00	1.10	898.55	320	108	99	1.000	69.3	2.850	113.8	
5-5	125	0.95	0.97	901.60	320	108	99	0.975	67.5	2.839	116.4	

Totals and Averages												
125		0.976	68.10	320		97.0		0.977	67.7	64.14	104.9	

Project Number	3648
Client	Big Rivers
Plant	Henderson
Location	Inlet
Date	8/4/2011
Tester ID	M-14
Y <sub>d</sub>	1.0087
Pitot C <sub>p</sub>	0.84

Place an "x" in the appropriate Box

Nozzle Diameter (in)	0.195
Filter ID	NA
Train Type	Impinger
Train ID	IB-10
P <sub>0</sub> (Inches Hg)	29.41
P <sub>s</sub> (Inches H <sub>2</sub> O)	-6.0
Start Time	10:09
Stop Time	12:38

Circular?	
Rectangular?	x
Diameter	
Length	186
Width	139

Moisture	Final Wt (g)	Tare Wt (g)	Net Wt (g)
Impinger 1	699.0	568.6	130.4
Impinger 2	716.3	698.6	17.7
Impinger 3	755.6	749.7	5.9
Impinger 4	742.2	635.1	107.1
Silica Gel	900.0	888.1	11.9
Weight of Water Collected, V <sub>w</sub> (g)			281.1
Silica Gel Net Weight, V <sub>wx</sub> (g)			11.9

CEMS	%CO <sub>2</sub>	%CO <sub>2</sub> -%O <sub>2</sub>	%O <sub>2</sub>
Average	12.2	NA	5.60

Run 2

Traverse Point	min/Pt	Velocity Pressure ΔP (in H <sub>2</sub> O)	Orifice Setting ΔH (in H <sub>2</sub> O)	Gas Sample Volume Initial (ft <sup>3</sup> )	Start Temp (°F)	DGM Inlet (°F)	DGM Outlet (°F)	Square Root ΔP	Stack Gas Velocity V <sub>s</sub> (ft/sec)	Volume Measured V <sub>mstd</sub> (ft <sup>3</sup> )	Isokinetics (%)
	5										
				902.40							
1-1	5	0.70	0.71	904.84	315	104	100	0.837	68.4	2.276	113.9
1-2	10	0.72	0.73	907.27	316	104	101	0.849	69.3	2.265	111.8
1-3	15	0.83	0.85	909.85	315	105	102	0.811	63.3	2.401	110.4
1-4	20	0.89	0.91	912.53	316	106	102	0.905	65.6	2.492	110.7
1-5	25	0.65	0.66	915.01	316	106	100	0.806	56.3	2.308	120.0
2-1	30	0.77	0.78	917.55	317	106	100	0.877	61.2	2.366	113.0
2-2	35	0.80	0.82	920.12	316	107	100	0.894	62.5	2.392	112.0
2-3	40	0.80	0.82	922.67	316	106	99	0.894	62.5	2.371	111.4
2-4	45	0.76	0.77	925.64	316	107	100	0.872	60.8	2.783	132.8
2-5	50	0.70	0.71	927.56	316	107	100	0.837	58.5	1.798	98.5
3-1	55	0.98	1.00	930.41	317	102	99	0.990	69.2	2.668	113.0
3-2	60	1.00	1.00	933.32	317	102	97	1.000	68.9	2.729	115.4
3-3	65	1.10	1.10	936.22	317	102	96	1.049	73.3	2.722	108.8
3-4	70	1.20	1.20	939.21	318	102	96	1.095	76.7	2.907	107.5
3-5	75	0.86	0.88	941.82	317	101	96	0.927	64.9	2.451	110.8
4-1	80	1.20	1.20	944.81	318	100	94	1.095	76.7	2.916	107.8
4-2	85	1.20	1.20	947.81	318	100	94	1.095	76.7	2.827	106.5
4-3	90	1.10	1.10	950.77	318	101	95	1.049	73.4	2.784	111.4
4-4	95	1.00	1.00	953.50	317	101	96	1.000	69.9	2.564	107.5
4-5	100	1.10	1.10	956.39	317	101	94	1.049	73.3	2.720	108.7
5-1	105	1.00	1.00	959.27	318	101	94	1.000	70.0	2.710	113.7
5-2	110	1.20	1.20	962.19	318	101	94	1.095	76.7	2.749	106.3
5-3	115	1.40	1.40	963.10	318	101	94	1.183	82.8	0.857	30.6
5-4	120	1.10	1.10	968.38	317	101	94	1.049	73.3	2.970	198.7
5-5	125	1.10	1.10	971.26	318	101	94	1.049	73.4	2.711	108.8

Totals and Averages											
	125		0.974	68.86	317		100	0.978	68.4	64.49	110.6

Project Number	3648
Client	Big Rivers
Plant	Henderson
Location	Inlet
Date	8/4/2011
Meter ID	M-14
% <sub>d</sub>	1.0087
Pitot C <sub>2</sub>	0.84

Place an "x" in the appropriate Box

Nozzle Diameter (in)	0.195
Filter ID	NA
Train Type	Impinger
Train ID	NEW
P <sub>1</sub> (Inches Hg)	29.41
P <sub>2</sub> (Inches H <sub>2</sub> O)	-6.0
Start Time	13:11
Stop Time	15:40

Circular?	
Rectangular?	x
Diameter	
Length	186
Width	139

Impinger	Final Wt (g)	Tare Wt (g)	Net Wt (g)
Impinger 1	632.9	621.2	11.7
Impinger 2	632.5	609.7	22.8
Impinger 3	726.0	711.0	15.0
Impinger 4	624.1	618.6	5.5
Silica Gel	940.0	919.5	20.5
Weight of Water Collected, V <sub>w</sub> (g)			155.1
Silica Gel Net Weight, W <sub>sil</sub> (g)			20.5

CEMS	%CO <sub>2</sub>	%CO <sub>2</sub> :%O <sub>2</sub>	%C <sub>2</sub>
Average	13.3	NA	3.44

Run 3

Traverse Point	Min/Ft	Velocity Pressure ΔP (in H <sub>2</sub> O)	Orifice Setting ΔH (in H <sub>2</sub> O)	Gas Sample Volume Ingal (ft <sup>3</sup> )	Stack Temp (°F)	DPM Inlet (°F)	DGM Outlet (°F)	Square Root ΔP	Stack Gas Velocity (ft/sec)	Volume Measured (ft <sup>3</sup> )	Isokinetics (%)
	5										
				972.10							
1-1	5	0.65	0.66	974.48	315	99	97	0.806	55.7	2.236	110.6
1-2	10	0.73	0.74	976.90	316	100	97	0.854	59.0	2.270	108.1
1-3	15	0.82	0.84	979.45	316	102	97	0.904	62.6	2.300	105.4
1-4	20	0.85	0.87	981.99	315	102	98	0.922	63.7	2.319	102.9
1-5	25	0.63	0.64	984.46	315	103	98	0.794	54.9	2.310	116.1
2-1	30	0.76	0.77	986.93	315	106	101	0.872	60.2	2.298	105.2
2-2	35	0.78	0.79	989.42	316	106	100	0.863	61.0	2.319	104.8
2-3	40	0.75	0.76	991.92	316	107	100	0.866	59.8	2.326	107.2
2-4	45	0.80	0.82	994.45	316	108	102	0.894	61.9	2.348	104.8
2-5	50	0.70	0.71	996.86	316	109	102	0.837	57.8	2.254	106.9
3-1	55	1.00	1.00	999.27	318	109	103	1.000	68.1	2.334	99.2
3-2	60	1.00	1.00	1002.12	318	110	103	1.000	69.1	2.639	105.4
3-3	65	1.10	1.10	1005.02	318	111	104	1.049	72.5	2.682	102.1
3-4	70	1.20	1.20	1007.83	316	112	104	1.095	75.7	2.687	94.6
3-5	75	0.87	0.89	1010.69	316	112	105	0.893	64.5	2.658	112.9
4-1	80	1.10	1.10	1013.52	316	111	105	1.049	72.5	2.614	98.5
4-2	85	1.10	1.10	1016.47	316	111	105	1.049	72.5	2.725	103.7
4-3	90	1.20	1.20	1019.50	316	112	106	1.095	75.7	2.785	101.9
4-4	95	1.00	1.00	1022.36	316	112	105	1.000	69.1	2.639	105.1
4-5	100	1.10	1.10	1025.22	316	112	105	1.049	72.5	2.640	100.5
5-1	105	1.30	1.30	1028.29	318	111	104	1.150	76.9	2.940	95.4
5-2	110	1.20	1.20	1031.42	316	111	104	1.095	75.7	2.695	105.5
5-3	115	1.50	1.50	1034.75	318	111	104	1.225	84.6	3.082	100.5
5-4	120	1.20	1.20	1037.84	316	111	104	1.095	75.7	2.859	102.1
5-5	125	1.00	1.00	1040.67	316	111	104	1.000	69.1	2.316	104.4

Totals and Averages

125	0.980	68.57	316	105	0.960	67.7	63.63	103.6
-----	-------	-------	-----	-----	-------	------	-------	-------

Project Number	3648
Client	Big Rivers
Plant	Henderson
Location	Unit 2 Inlet
Date	8/4/11
P <sub>3</sub> (Inches Hg)	29.41

Meter ID	M-26
Y <sub>6</sub>	0.9958

Start Time	7:19
Stop Time	9:58

Meter ID	M-26
Y <sub>6</sub>	0.9902

**Run 1**

Min/Pt	Gas Sample	DGM Temp (°F)	Volume Metered Vmstd (L)
3.6	Volume		
Elapsed Time	Initial (L)		
	0.00		
3.60	2.197	80	2.102
7.20	3.661	80	1.401
10.80	4.872	81	1.156
14.40	6.022	83	1.094
18.00	6.994	84	0.923
21.60	7.815	89	0.773
25.20	9.093	89	1.203
28.80	10.196	92	1.032
32.40	11.235	93	0.971
36.00	12.478	96	1.155
39.60	13.901	97	1.320
43.20	15.612	98	1.584
46.80	16.683	98	0.992
50.40	18.451	99	1.634
54.00	20.215	101	1.624
57.60	22.115	102	1.747
61.20	24.723	102	2.397
64.80	27.449	103	2.501
68.40	29.650	103	2.020
72.00	32.253	104	2.384
75.60	34.674	105	2.214
79.20	36.955	106	2.082
82.80	40.831	107	3.532
86.40	42.573	108	1.584
90.00	43.547		1.094

**Totals and Averages**

90	43.547	95.8	40.47
----	--------	------	-------

**Run 1 Spiked**

Min/Pt	Gas Sample	DGM Temp (°F)	Volume Metered Vmstd (L)
3.6	Volume		
Elapsed Time	Initial (L)		
	0.00		
3.6	2.113	80	2.010
7.2	3.385	81	1.208
10.8	4.494	82	1.051
14.4	5.723	84	1.161
18.0	6.821	87	1.031
21.6	7.772	91	0.887
25.2	9.171	92	1.302
28.8	10.291	93	1.040
32.4	11.397	95	1.024
36.0	12.593	97	1.103
39.6	13.993	98	1.289
43.2	15.721	99	1.588
46.8	16.814	100	1.003
50.4	18.630	101	1.663
54.0	20.523	103	1.727
57.6	22.190	103	1.521
61.2	24.352	104	1.969
64.8	26.689	104	2.129
68.4	29.036	106	2.130
72.0	32.088	106	2.770
75.6	35.171	107	2.793
79.2	37.949	107	2.517
82.8	41.105	108	2.854
86.4	42.001	109	0.809
90.0	43.297		1.447

**Totals and Averages**

90	43.297	97.4	39.90
----	--------	------	-------

Project Number	3648
Client	Big Rivers
Plant	Henderson
Location	Unit 2 Inlet
Date	8/4/11
F <sub>b</sub> (Inches Hg)	29.41

Meter ID	M-26
Y <sub>d</sub>	0.9958

Start Time	10:09
Stop Time	11:54

Meter ID	M-26
Y <sub>n</sub>	0.9902

**Run 2**

Min/Pt	Gas Sample	DGM Temp (°F)	Volume Metered Vrnstd (L)
3.6	Volume Initial (L)		
Elapsed Time	0.000		
3.6	2.257	94	2 105
7.2	3.486	94	1 146
10.8	4.412	94	0 864
14.4	5.516	94	1 029
18.0	6.695	96	1 095
21.6	7.496	98	0 742
25.2	9.029	99	1 417
28.8	10.350	101	1 216
32.4	12.467	102	1 946
36.0	13.803	104	1 224
39.6	15.741	104	1 775
43.2	17.382	105	1 500
46.8	19.372	107	1 813
50.4	20.858	108	1 352
54.0	22.709	108	1 684
57.6	24.274	108	1 423
61.2	26.315	109	1 853
64.8	27.976	109	1 508
68.4	29.763	110	1 620
72.0	31.328	111	1 416
75.6	32.932	110	1 454
79.2	35.671	111	2 478
82.8	36.901	111	1 113
86.4	39.244	111	2 120
90.0	42.276		3 405

**Run 2 Spiked**

Min/Pt	Gas Sample	DGM Temp (°F)	Volume Metered Vrnstd (L)
3.6	Volume Initial (L)		
Elapsed Time	0.00		
3.6	2.055	94	1 906
7.2	3.146	94	1 012
10.8	4.443	94	1 203
14.4	6.037	95	1 475
18.0	7.456	97	1 309
21.6	8.079	100	0 572
25.2	9.015	101	0 857
28.8	10.649	103	1 491
32.4	12.731	103	1 900
36.0	14.945	105	2 013
39.6	16.173	106	1 115
43.2	17.167	108	0 999
46.8	18.978	109	1 635
50.4	20.167	110	1 072
54.0	22.124	110	1 764
57.6	23.927	111	1 622
61.2	26.067	111	1 925
64.8	27.935	111	1 681
68.4	29.814	112	1 688
72.0	31.648	112	1 647
75.6	33.532	111	1 695
79.2	36.212	112	2 407
82.8	37.311	112	0 987
86.4	39.403	112	1 879
90.0	42.045		2 950

**Totals and Averages**

90	42.276	104	38.72
----	--------	-----	-------

**Totals and Averages**

90	42.045	106	38.19
----	--------	-----	-------

Project Number	3648
Client	Big Rivers
Plant	Henderson
Location	Unit 2 Inlet
Date	8/4/11
P <sub>b</sub> (Inches Hg)	29.41

Meter ID	M-26
Y <sub>d</sub>	0.9958

Start Time	13:11
Stop Time	15:54

Meter ID	M-26
Y <sub>j</sub>	0.9902

**Run 3**

Min/Pt	Gas Sample	DGM Temp (°F)	Volume Metered Vmstd (L)
3.6	Volume Initial (L)		
Elapsed Time	0.00		
3.6	1.658	94	1.546
7.2	3.327	95	1.554
10.8	4.549	95	1.137
14.4	6.051	96	1.396
18.0	7.645	97	1.478
21.6	9.181	99	1.420
25.2	10.549	101	1.260
28.8	11.986	103	1.319
32.4	13.410	104	1.304
36.0	15.198	106	1.632
39.6	16.667	107	1.338
43.2	17.893	108	1.115
46.8	19.321	109	1.297
50.4	20.801	111	1.339
54.0	22.161	111	1.230
57.6	23.966	113	1.627
61.2	25.007	114	0.937
64.8	26.430	116	1.276
68.4	28.963	115	2.276
72.0	32.006	115	2.734
75.6	33.700	115	1.522
79.2	35.434	116	1.555
82.8	36.153	117	0.644
86.4	37.190	117	0.928
90.0	40.816		4.072

**Totals and Averages**

90	40.816	107	37.17
----	--------	-----	-------

**Run 3 Spiked**

Min/Pt	Gas Sample	DGM Temp (°F)	Volume Metered Vmstd (L)
3.6	Volume Initial (L)		
Elapsed Time	0.00		
3.6	2.394	94	2.220
7.2	2.820	95	0.394
10.8	4.431	95	1.491
14.4	6.189	96	1.624
18.0	8.026	97	1.894
21.6	9.386	101	1.245
25.2	10.783	102	1.277
28.8	12.126	105	1.221
32.4	13.363	106	1.123
36.0	14.843	108	1.339
39.6	16.173	109	1.201
43.2	17.491	111	1.186
46.8	18.765	112	1.144
50.4	20.300	113	1.376
54.0	21.673	113	1.231
57.6	22.051	115	0.338
61.2	24.962	116	2.596
64.8	26.727	117	1.571
68.4	28.726	117	1.780
72.0	30.753	118	1.802
75.6	32.178	118	1.266
79.2	34.102	118	1.710
82.8	35.982	119	1.668
86.4	37.378	119	1.239
90.0	41.009		4.055

**Totals and Averages**

90	41.009	109	37.03
----	--------	-----	-------

Project Number	3648
Client	Big Rivers
Plant	Henderson
Location	Unit 2 Stack
Date	8/4/2011
Filter ID	M-17
$V_c$	1.0141
$P_{col} C_c$	0.84

Place an "x" in the appropriate Box

Circular?	x
Rectangular?	
Diameter	192
Length	
Width	

Moisture	Final Wt (g)	Tare Wt (g)	Net Wt (g)
Impinger 1	632.6	526.2	106.4
Impinger 2	629.4	706.7	-77.3
Impinger 3	724.4	609.6	114.8
Silica Gel	924.7	890.0	34.7
Weight of Water Collected $W_{col}$ (g)			145.9
Silica Gel Net Weight $W_{net}$ (g)			34.7

Nozzle Diameter (in)	0.230
Filter ID	12149
Train Type	Impinger
Train ID	IB-4
$P_b$ (Inches Hg)	29.41
$P_c$ (Inches H <sub>2</sub> O)	-0.4
Start Time	7:19
Stop Time	9:03

CEMS	%CO <sub>2</sub>	%CO <sub>2</sub> +%O <sub>2</sub>	%O <sub>2</sub>
Average	12.9	NA	8.20

Run 1

Traverse Point	min/Pt	Velocity Pressure $\Delta P$ (in H <sub>2</sub> O)	Orifice Setting $\Delta H$ (in H <sub>2</sub> O)	Gas Sample Volume Initial (ft <sup>3</sup> )	Stack Temp (°F)	DGR Inlet (°F)	DGR Outlet (°F)	Square Foot $\Delta F$	Stack Gas Velocity $V_s$ (ft/sec)	Volume Measured (ft <sup>3</sup> )	Isokinetic (%)
	7.5										
4-1	7.5	0.61	1.30	75.22	129	99	99	0.781	27.1	2.542	99.1
4-2	15.0	0.55	1.20	79.72	129	102	99	0.742	24.7	2.237	97.3
4-3	22.5	0.24	0.53	82.53	129	104	99	0.690	28.5	2.536	91.7
1-1	30.0	0.65	1.40	87.38	130	106	100	0.806	28.6	2.548	96.3
1-2	37.5	0.59	1.30	92.23	130	108	101	0.768	26.3	2.542	100.9
1-3	45.0	0.30	0.66	95.53	131	108	101	0.548	32.1	3.001	96.0
2-1	52.5	0.82	1.40	99.64	130	109	102	0.787	27.5	2.637	83.1
2-2	60.0	0.57	1.30	105.03	129	110	103	0.755	25.5	2.522	112.4
2-3	67.5	0.32	0.70	108.51	130	110	103	0.566	34.1	3.239	97.7
3-1	75.0	0.84	1.40	113.34	130	111	104	0.800	26.2	2.499	95.8
3-2	82.5	0.81	1.30	118.49	129	111	104	0.781	27.1	2.790	104.8
3-3	90.0	0.43	0.95	122.42	130	112	105	0.656	39.5	3.646	94.3

Totals and Averages

90	1.12	52.01	130	105	0.707	42.6	48.61	97.8
----	------	-------	-----	-----	-------	------	-------	------

Project Number	3648
Client	Big Rivers
Plant	Henderson
Location	Unit 2 Stack
Date	8/4/2011
Meter ID	M-17
Y <sub>2</sub>	1.0141
Pitot C <sub>p</sub>	0.84

Place an "X" in the appropriate Box

Circular?	<input checked="" type="checkbox"/>
Rectangular?	<input type="checkbox"/>
Diameter	192
Length	
Width	

Moisture	Final Wt. (g)	Tare Wt. (g)	Net Wt. (g)
Impinger 1	657.5	546.6	110.9
Impinger 2	709.9	677.2	32.7
Impinger 3	655.7	628.3	27.4
Silica Gel	932.2	910.5	21.7
Weight of Water Collected, V <sub>w</sub> (g)			171.0
Silica Gel Net Weight, V <sub>sil</sub> (g)			21.7

Nozzle Diameter (in)	0.230
Filter ID	12150
Train Type	Impinger
Train ID	IB-3
F <sub>s</sub> (Inches Hg)	29.41
F <sub>o</sub> (Inches H <sub>2</sub> O)	-0.4
Start Time	10:08
Stop Time	11:57

CEMS	%CO <sub>2</sub>	%CO <sub>2</sub> +%O <sub>2</sub>	%O <sub>2</sub>
Average	12.8	NA	6.00

Run 2

Traverse Point	Man/pt	Velocity Pressure ΔP (in H <sub>2</sub> O)	Orifice Setting ΔH (in H <sub>2</sub> O)	Gas Sample Volume Initial (ft <sup>3</sup> )	Stack Temp (°F)	DGM Inlet (°F)	DGM Outlet (°F)	Square Root ΔP	Stack Gas Velocity Vs (ft/sec)	Volume Metered (ft <sup>3</sup> )	Isokinetic (%)
	7.5										
4-1	7.5	0.62	1.40	127.84	129	110	108	0.787	47.5	4.537	99.2
4-2	15.0	0.54	1.20	132.47	129	117	108	0.735	44.3	4.268	100.0
4-3	22.5	0.24	0.53	135.50	131	118	110	0.690	29.6	2.781	97.9
1-1	30.0	0.67	1.50	140.60	130	119	110	0.915	49.4	4.688	96.7
1-2	37.5	0.58	1.30	145.35	129	119	110	0.762	45.9	4.364	98.7
1-3	45.0	0.29	0.64	148.74	130	119	110	0.536	32.5	3.109	98.5
2-1	52.5	0.62	1.40	153.77	130	119	111	0.787	47.5	4.618	101.1
2-2	60.0	0.58	1.30	158.58	130	119	111	0.762	48.0	4.397	99.5
2-3	67.5	0.32	0.71	162.10	131	119	111	0.560	34.2	3.245	98.9
3-1	75.0	0.64	1.40	167.05	130	120	111	0.900	48.5	4.541	97.8
3-2	82.5	0.62	1.40	171.94	129	120	112	0.787	47.5	4.482	96.0
3-3	90.0	0.42	0.93	175.91	130	120	112	0.646	36.1	3.662	97.2

Totals and Averages

90		1.14	52.99	130	114	0.707	42.7	48.68	98.5
----	--	------	-------	-----	-----	-------	------	-------	------

Project Number	3648
Client	Big Rivers
Plant	Henderson
Location	Unit 2 Stack
Date	8/4/2011
Filter ID	AL-17
Y <sub>1</sub>	1.0141
Filter C <sub>p</sub>	0.84

Place an "x" in the appropriate Box

Circular	x
Rectangular?	
Diameter	192
Length	
Width	

Impinger	Final Wt (g)	Tare Wt (g)	Net Wt (g)
Impinger 1	694.1	568.1	126.0
Impinger 2	750.0	708.4	41.6
Impinger 3	548.9	525.1	23.8
Silica Gel	935.7	924.7	11.0
Weight of Water Collected, W <sub>3</sub> (g)			181.4
Silica Gel Net Weight, W <sub>3</sub> (g)			11.0

Nozzle Diameter (in)	0.230
Filter ID	12151
Train Type	Impinger
Train ID	IB-4
P <sub>0</sub> (Inches Hg)	29.41
P <sub>1</sub> (Inches H <sub>2</sub> O)	-0.4
Start Time	13:11
Stop Time	15:06

CEMS	%CO <sub>2</sub>	%CO <sub>2</sub> +%O <sub>2</sub>	%O <sub>2</sub>
Average	13.1	NA	5.67

Run 3

Traverse Point	Min/Pl	Velocity Pressure ΔP (in. H <sub>2</sub> O)	Orifice Setting ΔH (in. H <sub>2</sub> O)	Gas Sample Volume Initial (ft <sup>3</sup> )	Stack Temp (°F)	DGM Inlet (°F)	DGM Outlet (°F)	Squire Rnot ΔP	Stack Gas Velocity V <sub>s</sub> (ft/sec)	Volume Metered V <sub>metd</sub> (ft <sup>3</sup> )	Isokinetic (%)
	7.5 Elapsed Time										
4-1	7.5	0.63	1.40	182.63	129	113	109	0.794	47.9	4466	98.3
4-2	15.0	0.55	1.20	188.96	130	115	109	0.742	44.8	3932	139.9
4-3	22.5	0.23	0.52	190.20	130	117	110	0.480	28.9	1139	41.5
1-1	30.0	0.67	1.50	194.69	130	118	110	0.819	49.4	4131	88.0
1-2	37.5	0.56	1.30	191.36	131	118	110	0.748	45.2	3022	-71.6
1-3	45.0	0.30	0.68	202.73	130	118	110	0.548	33.1	10439	333.3
2-1	52.5	0.61	1.40	207.29	130	118	110	0.781	47.1	4194	83.9
2-2	60.0	0.59	1.30	211.42	129	118	111	0.762	46.3	3794	96.3
2-3	67.5	0.32	0.72	214.90	130	118	111	0.586	34.1	3193	98.7
3-1	75.0	0.63	1.40	220.12	130	118	111	0.794	47.9	4737	105.7
3-2	82.5	0.63	1.40	224.59	131	118	111	0.794	47.9	4108	90.6
3-3	90.0	0.41	0.93	228.63	130	118	112	0.640	38.0	3705	101.2

Totals and Averages

90	1.16	50.93	130	114	0.706	42.6	46.83	94.9
----	------	-------	-----	-----	-------	------	-------	------

Project Number	3648
Client	Big Rivers
Plant	Henderson
Location	Unit 2 Stack
Date	8/4/2011
Meier ID	M-15
Y <sub>d</sub>	1.0159
Pitot C <sub>p</sub>	0.84

Place an "x" in the appropriate Box

Circular?	x
Rectangular?	
Diameter	192
Length	
Width	

Nozzle Diameter (in)	0.270
Filter ID	NA
Train Type	Impingers
Train ID	IB-9
P <sub>h</sub> (Inches Hg)	29.41
P <sub>s</sub> (Inches H <sub>2</sub> O)	-0.4
Start Time	7:19
Stop Time	9:23

Impinger	Final Wt (g)	Tare Wt (g)	Net Wt (g)
Impinger 1	846.3	616.5	229.9
Impinger 2	652.0	618.5	33.5
Impinger 3	539.5	530.5	9.0
Silica Gel	928.0	912.2	15.8
Weight of Water Collected, W <sub>w</sub> (g)			272.3
Silica Gel Net Weight, W <sub>sg</sub> (g)			15.8

CEMS	%CO <sub>2</sub>	%CO <sub>2</sub> +%O <sub>2</sub>	%O <sub>2</sub>
Average	12.8	NA	6.20

Run 1

Travel Point	Mir/P.	Velocity Pressure ΔP (in H <sub>2</sub> O)	Orifice Setting ΔH (in H <sub>2</sub> O)	Gas Sample Volume Initial (ft <sup>3</sup> )	Stack Temp (°F)	DGM Inlet (°F)	DGM Outlet (°F)	Square Root ΔP	Stack Gas Velocity (ft/sec)	Volume Metered (ft <sup>3</sup> )	Isokinence (%)
	10 Elapsed Time										
				867.54							
1-1	10	0.60	2.60	876.34	129	100	98	0.775	46.6	9.351	99.1
1-2	20	0.56	2.40	884.74	130	105	98	0.748	45.0	7.832	97.5
1-3	30	0.31	1.30	890.89	130	110	100	0.557	33.5	5.755	95.1
2-1	40	0.59	2.50	898.96	130	112	102	0.768	46.2	7.548	97.4
2-2	50	0.52	2.20	906.99	130	112	103	0.721	43.4	7.499	95.7
2-3	60	0.28	1.20	914.22	130	115	104	0.528	21.6	6.711	116.7
3-1	70	0.57	2.50	921.77	130	119	106	0.755	45.4	6.981	88.3
3-2	80	0.51	2.20	929.23	130	120	107	0.711	45.0	6.993	88.8
3-3	90	0.28	1.20	935.49	130	118	108	0.528	31.8	5.773	100.4
4-1	100	0.50	2.20	943.82	130	116	108	0.707	42.5	7.717	100.1
4-2	110	0.46	1.90	952.53	130	116	108	0.678	40.8	9.064	105.4
4-3	120	0.27	1.20	958.50	130	116	109	0.520	31.3	5.512	97.6

Totals and Averages

120	1.95	90.96	130	109	0.667	40.1	84.70	97.4
-----	------	-------	-----	-----	-------	------	-------	------

Project Number	3648
Client	Big Rivers
Plant	Henderson
Location	Unit 2 Stack
Date	8/4/2011
Meter ID	M-15
Yr	1.0159
Pilot Cp	0.84

Place an "x" in the appropriate Box

Nozzle Diameter (in)	0.270
Filter ID	NA
Train Type	Impingers
Train ID	IB
P <sub>1</sub> (Inches Hg)	29.41
P <sub>2</sub> (Inches H <sub>2</sub> O)	-0.4
Start Time	10:08
Stop Time	12:31

Circular?	x
Rectangular?	
Diameter	102
Length	
Width	

Impinger	Final Wt (g)	Tare Wt (g)	Net Wt (g)
Impinger 1	874.2	717.3	156.9
Impinger 2	702.0	688.1	13.9
Impinger 3	596.8	589.3	7.5
Silica Gel	855.0	846.0	9.0
Weight of Water Collected, V <sub>w</sub> (g)			178.3
Silica Gel Net Weight, V <sub>silica</sub> (g)			9.0

CEMS	%CO <sub>2</sub>	%CO <sub>2</sub> +%O <sub>2</sub>	%O <sub>2</sub>
Average	12.6	NA	6.00

Run 2

Traverse Point	Min/Fl	Velocity Pressure ΔP (in H <sub>2</sub> O)	Orifice Setting ΔH (in H <sub>2</sub> O)	Gas Sample Volume Initial (ft <sup>3</sup> )	Stack Temp (°F)	DGM Inlet (°F)	Orifice Outlet (°F)	Square Root ΔP	Stack Gas Velocity V <sub>s</sub> (ft/sec)	Volume Metered (ft <sup>3</sup> )	Isokinetic (%)
	10										
				959.03							
1-1	10	0.60	2.60	967.60	130	104	104	0.775	46.1	8.060	91.7
1-2	20	0.52	2.20	975.88	130	104	103	0.721	42.0	7.787	95.1
1-3	30	0.27	1.20	981.73	129	107	103	0.520	30.9	5.473	92.7
2-1	40	0.61	2.60	990.64	129	110	103	0.781	46.5	8.345	94.0
2-2	50	0.54	2.30	999.55	129	110	104	0.735	45.7	8.330	96.8
2-3	60	0.28	1.20	1005.97	129	112	104	0.529	31.5	5.975	96.4
3-1	70	0.61	2.60	1014.83	129	114	105	0.781	46.5	8.253	93.0
3-2	80	0.63	2.30	1023.67	129	116	105	0.726	43.9	8.121	98.2
3-3	90	0.29	1.30	1029.83	129	116	106	0.539	32.1	5.797	94.7
4-1	100	0.62	2.70	1036.42	129	117	106	0.747	46.3	6.115	68.4
4-2	110	0.53	2.30	1048.05	129	117	106	0.726	43.9	10.797	100.0
4-3	120	0.28	1.20	1054.22	130	117	106	0.529	31.5	6.707	96.0

Totals and Averages

120			2.04	95.19	129	108		0.679	40.4	88.73	95.8
-----	--	--	------	-------	-----	-----	--	-------	------	-------	------

Project Number	3648
Client	Big Rivers
Plant	Henderson
Location	Unit 2 Stack
Date	8/4/2011
Meier ID	M-15
Yr	1,0159
Flot Cp	0.84

Place an "x" in the appropriate Box

Nozzle Diameter (in)	0.270
Filter ID	NA
Train Type	Impingers
Train ID	IB-9
F <sub>h</sub> (Inches Hg)	29.41
F <sub>w</sub> (Inches H <sub>2</sub> O)	-0.4
Start Time	13:11
Stop Time	15:36

Circular?	x
Rectangular?	
Diameter	192
Length	
Width	

Moisture	Final Wt (g)	Tare Wt (g)	Net Wt (g)
Impinger 1	807.5	619.3	188.2
Impinger 2	651.3	619.7	31.6
Impinger 3	539.2	529.1	10.1
Silica Gel	942.2	927.2	15.0
Weight of Water Collected V <sub>15</sub> (g)			229.9
Silica Gel Net Weight V <sub>25</sub> (g)			15.0

CEMS	%CO <sub>2</sub>	%CO <sub>2</sub> +%O <sub>2</sub>	%O <sub>2</sub>
Average	13.1	NA	5.67

Run 3

Transverse Point	Min/Pt	Velocity Pressure ΔP (in H <sub>2</sub> O)	Orifice Setting ΔH (in H <sub>2</sub> O)	Gas Sample Volume Inlet (ft <sup>3</sup> )	Stack Temp (°F)	DGM Inlet (°F)	DGM Outlet (°F)	Square Root ΔP	Stack Gas Velocity V <sub>s</sub> (ft/sec)	Volume Meter V <sub>m</sub> (ft <sup>3</sup> )	Isokinetic (%)
	10 Elapsed Time										
1-1	10	0.61	2.70	63.99	130	105	105	0.761	46.7	8.574	98.4
1-2	20	0.54	2.40	72.72	129	110	105	0.735	43.9	8.156	99.8
1-3	30	0.27	1.20	78.92	130	114	105	0.520	31.1	5.755	99.7
2-1	40	0.60	2.60	87.98	130	115	106	0.775	46.4	8.424	97.9
2-2	50	0.55	2.40	96.51	129	116	107	0.742	44.3	7.914	96.0
2-3	60	0.26	1.10	101.21	129	117	107	0.510	30.5	4.342	79.6
3-1	70	0.61	2.70	111.86	129	117	107	0.781	46.7	9.879	112.8
3-2	80	0.52	2.30	121.06	129	117	108	0.721	43.1	8.518	106.3
3-3	90	0.25	1.10	127.04	129	117	108	0.500	29.9	5.320	98.3
4-1	100	0.60	2.60	135.85	129	117	107	0.775	46.3	8.170	94.9
4-2	110	0.53	2.30	145.11	130	117	107	0.729	43.6	8.581	106.1
4-3	120	0.22	0.97	151.43	129	117	107	0.466	28.0	5.837	111.9

Totals and Averages

120		2.03	96.57	129	111	0.670	40.0	89.63	100.4
-----	--	------	-------	-----	-----	-------	------	-------	-------

Project Number	3648
Client	Big Rivers
Plant	Henderson
Location	Unit 2 Stack
Date	8/4/2011
Meter ID	M-16
$V_4$	0.9907
Filter $C_1$	0.84

Place an "x" in the appropriate Box

Circular?	x
Rectangular?	
Diameter	192
Length	
Width	

Impinger	Final Wt (g)	Tare Wt (g)	Net Wt (g)
Impinger 1	825.8	624.9	200.9
Impinger 2	623.0	604.8	18.2
Impinger 3	674.0	697.5	-23.5
Impinger 4	709.5	643.0	66.5
Silica Gel	937.1	912.0	25.1
Weight of Water Collected $V_{w3}$ (g)			262.1
Silica Gel Net Weight $V_{w3g}$ (g)			25.1

Nozzle Diameter (in)	0.230
Filter ID	NA
Train Type	Impinger
Train ID	IB
$P_1$ (Inches Hg)	29.41
$P_2$ (Inches H <sub>2</sub> O)	-0.4
Start Time	7:19
Stop Time	9:23

CEMS	%CO <sub>2</sub>	%CO <sub>2</sub> +%O <sub>2</sub>	%O <sub>2</sub>
Average	12.2	NA	6.20

Run 1

Traverse Point	10	Velocity Pressure ΔP (in H <sub>2</sub> O)	Orifice Setting ΔH (in H <sub>2</sub> O)	Gas Sample Volume Initial (ft <sup>3</sup> )	Stack Temp (°F)	DGM Inlet (°F)	DGM Outlet (°F)	Square Root ΔP	Stack Gas Velocity V <sub>s</sub> (ft/sec)	Volume Metered V <sub>m</sub> (ft <sup>3</sup> )	Isokinetics (%)
	Elapsed Time										
4-1	10	0.64	1.50	398.83	129	97	97	0.800	48.2	6.196	101.8
4-2	20	0.60	1.40	405.56	130	100	97	0.775	46.7	6.215	105.5
4-3	30	0.42	0.97	411.07	129	104	98	0.648	38.1	5.060	102.6
3-1	40	0.65	1.50	418.01	129	106	98	0.806	48.6	6.371	103.2
3-2	50	0.57	1.30	424.39	129	109	100	0.755	45.5	5.928	101.4
3-3	60	0.30	0.69	429.05	128	110	101	0.546	23.0	4.243	101.7
2-1	70	0.61	1.40	435.70	129	112	102	0.781	47.1	6.045	101.8
2-2	80	0.55	1.30	442.10	129	110	103	0.742	44.7	5.625	103.2
2-3	90	0.32	0.74	446.93	129	109	103	0.566	34.1	4.392	102.1
1-1	100	0.59	1.40	453.50	130	108	103	0.768	46.3	5.992	102.6
1-2	110	0.54	1.20	459.57	130	109	103	0.735	44.3	5.529	98.3
1-3	120	0.25	0.58	463.85	129	110	103	0.600	30.1	3.989	102.2

Totals and Averages

120	1.17	71.71	129	104	0.702	42.3	65.56	99.8
-----	------	-------	-----	-----	-------	------	-------	------

Project Number	3648
Client	Big Rivers
Plant	Henderson
Location	Unit 2 Stack
Date	8/4/2011
Meter ID	M-16
Yd	0.9907
Pitot Cp	0.84

Place an "x" in the appropriate Box

Circular?	x
Rectangular?	
Diameter	192
Length	
Width	

Nozzle Diameter (in)	0.230
Filter ID	NA
Train Type	Impinger
Train ID	IB24
P <sub>1</sub> (Inches Hg)	29.41
P <sub>2</sub> (Inches H <sub>2</sub> O)	-0.4
Start Time	10:08
Stop Time	12:31

Moisture	Final Wt (g)	Tare Wt (g)	Net Wt (g)
Impinger 1	774.2	588.4	187.8
Impinger 2	647.0	609.4	37.6
Impinger 3	630.0	612.1	17.9
Impinger 4	557.4	547.7	9.7
Silica Gel	924.0	909.7	14.3
Weight of Water Collected, W <sub>42</sub> (g)			
Silica Gel Net Weight, W <sub>40</sub> (g)	14.3		

CEMS	%CO <sub>2</sub>	%CO <sub>2</sub> +%O <sub>2</sub>	%C <sub>2</sub>
Average	12.8	NA	6.00

Run 2

Traverse Point	Min/Ft	Velocity Pressure ΔP (in H <sub>2</sub> O)	Orifice Setting ΔH (in H <sub>2</sub> O)	Gas Sample Volume Initial (ft <sup>3</sup> )	Stack Temp (°F)	DGM Inlet (°F)	DGM Outlet (°F)	Square Foot Area	Stack Gas Velocity (ft/sec)	Volume Metered (ft <sup>3</sup> )	Isokinetics (%)
	10 Elapsed Time										
4-1	10	0.62	1.40	464.38	130	102	99	0.787	47.5	7.946	129.1
4-2	20	0.59	1.40	479.64	129	103	99	0.766	46.3	6.187	104.2
4-3	30	0.41	0.94	485.02	129	109	100	0.830	38.6	6.910	98.2
3-1	40	0.60	1.40	491.69	129	110	102	0.775	46.7	6.078	101.5
3-2	50	0.57	1.30	498.02	129	111	103	0.756	45.5	5.757	98.6
3-3	60	0.33	0.76	502.87	129	111	103	0.574	34.6	4.405	99.2
2-1	70	0.60	1.40	509.81	130	110	103	0.775	46.8	6.136	102.6
2-2	80	0.56	1.30	516.07	129	112	103	0.746	45.1	5.870	101.5
2-3	90	0.35	0.81	521.07	129	113	104	0.592	35.7	4.530	99.0
1-1	100	0.62	1.40	527.75	130	112	104	0.787	47.5	6.066	99.7
1-2	110	0.53	1.20	533.83	130	112	104	0.729	35.9	5.518	98.1
1-3	120	0.23	0.53	537.95	129	113	105	0.480	26.9	3.726	100.5

Totals and Averages

120		1.15	73.57	129	106	0.701	42.3	66.98	102.2
-----	--	------	-------	-----	-----	-------	------	-------	-------

Project Number	3648
Client	Big Rivers
Plant	Henderson
Location	Unit 2 Stack
Date	8/4/2011
Meter ID	M-16
V <sub>g</sub>	0.9907
P <sub>std</sub> C <sub>p</sub>	0.84

Place an "x" in the appropriate Box

Circular?	x
Rectangular?	
Diameter	192
Length	
Width	

Moisture	Final Wt (g)	Tara Wt (g)	Net Wt (g)
Impinger 1	816.3	621.9	194.4
Impinger 2	646.0	607.6	38.4
Impinger 3	722.4	700.0	22.4
Impinger 4	655.0	645.1	9.9
Silica Gel	954.5	936.8	17.7
Weight of Water Collected, V <sub>w</sub> (g)			265.1
Silica Gel Net Weight, V <sub>sil</sub> (g)			17.7

Nozzle Diameter (in)	0.230
Filter ID	NA
Train Type	Impinger
Train ID	IB
P <sub>1</sub> (Inches Hg)	29.41
P <sub>2</sub> (Inches H <sub>2</sub> O)	-0.4
Start Time	13:11
Stop Time	15:00

CEMS	%CO <sub>2</sub>	%CO <sub>2</sub> +%O <sub>2</sub>	%C <sub>2</sub>
Average	13.1	NA	5.6

Run 3

Traverse Point	Min/Pl	Velocity Pressure Δ P (in H <sub>2</sub> O)	Orifice Setting Δ H (in H <sub>2</sub> O)	Gas Sample Volume Initial (ft <sup>3</sup> )	Stack Temp (°F)	DGM Inlet (°F)	DGM Outlet (°F)	Square Root Δ P	Stack Gas Velocity V <sub>s</sub> (ft/sec)	Volume Measured V <sub>std</sub> (ft <sup>3</sup> )	Isokinetic (%)
	10 Elapsed Time										
				538.13							
4-1	10	0.64	1.50	544.92	129	102	102	0.800	48.2	6.232	101.9
4-2	20	0.60	1.40	551.62	129	107	102	0.775	46.7	6.122	102.4
4-3	30	0.42	0.97	557.07	129	109	102	0.645	35.1	4.965	100.2
3-1	40	0.66	1.50	564.02	130	111	103	0.812	49.0	6.324	101.9
3-2	50	0.57	1.30	570.45	129	113	103	0.755	45.5	5.837	101.2
3-3	60	0.30	0.69	575.08	129	112	104	0.578	33.0	4.197	100.2
2-1	70	0.60	1.40	581.74	129	111	104	0.775	46.7	6.053	102.2
2-2	80	0.54	1.20	587.93	129	113	105	0.735	44.2	5.805	99.9
2-3	90	0.31	0.71	592.90	128	112	105	0.557	33.5	4.501	105.7
1-1	100	0.61	1.40	599.29	130	113	105	0.781	47.1	5.792	97.1
1-2	110	0.58	1.30	605.71	130	114	105	0.762	45.9	5.213	100.0
1-3	120	0.41	0.94	611.19	129	114	106	0.640	38.6	4.955	101.2

Totals and Averages

120	1.19	73.06	129	107	0.716	43.1	66.38	99.2
-----	------	-------	-----	-----	-------	------	-------	------

Project Number	3648
Client	Big Rivers
Plant	Henderson
Location	Stack
Date	8/4/11
P <sub>b</sub> (Inches Hg)	29.41

Meter ID	R20078
Y <sub>d</sub>	1.0072

Start Time	7:19
Stop Time	9:04

Meter ID	R20078
Y <sub>d</sub>	0.9985

**Run 1**

Min/Pt	Gas Sample	DGM Temp (°F)	Volume Metered Vmstd (L)
5	Volume Initial (L)		
Elapsed Time	0.00		
5.00	2.019	98	1 891
10.00	4.017	99	1 868
15.00	5.991	99	1 845
20.00	8.063	101	1 930
25.00	10.023	104	1 816
30.00	12.081	105	1 903
35.00	14.118	108	1 874
40.00	16.055	110	1 776
45.00	18.086	111	1 859
50.00	20.042	113	1 784
55.00	22.008	114	1 790
60.00	24.051	115	1 857
65.00	26.067	116	1 829
70.00	28.023	117	1 771
75.00	30.052	118	1 834
80.00	32.091	119	1 840
85.00	34.082	120	1 794
90.00	36.074	120	1 795

**Run 1 Spiked**

Min/Pt	Gas Sample	DGM Temp (°F)	Volume Metered Vmstd (L)
5	Volume Initial (L)		
Elapsed Time	0.00		
5	2.048	98	1 901
10	3.994	98	1 807
15	5.981	100	1 838
20	8.016	102	1 876
25	10.027	105	1 844
30	12.071	107	1 867
35	14.094	110	1 838
40	16.071	111	1 794
45	17.994	113	1 738
50	20.101	115	1 898
55	22.066	116	1 767
60	24.014	117	1 749
65	26.062	118	1 835
70	28.059	118	1 790
75	30.068	120	1 794
80	32.032	120	1 754
85	34.031	121	1 782
90	36.085	121	1 831

**Totals and Averages**

90	36.074	110	33.05
----	--------	-----	-------

**Totals and Averages**

90	36.085	112	32.70
----	--------	-----	-------

Project Number	3648
Client	Big Rivers
Plant	Henderson
Location	Stack
Date	8/4/11
P <sub>s</sub> (Inches Hg)	29.41

Meter ID	R20078
Y <sub>d</sub>	1.0072

Start Time	10:08
Stop Time	11:56

Meter ID	R20078
Y <sub>s</sub>	0.9985

**Run 2**

Min/Pt	Gas Sample	DGM Temp (°F)	Volume Metered Vrnstd (L)
5	Volume		
Elapsed Time	Initial (L)		
	0.00		
5	2.017	102	1.875
10	4.063	102	1.902
15	6.087	104	1.875
20	8.103	105	1.864
25	9.989	106	1.741
30	12.067	108	1.912
35	14.109	109	1.875
40	16.036	111	1.763
45	18.049	111	1.842
50	20.062	113	1.836
55	22.031	113	1.796
60	24.043	114	1.832
65	26.044	115	1.818
70	28.049	116	1.819
75	30.029	116	1.796
80	31.997	117	1.782
85	34.046	117	1.856
90	36.041	117	1.807

**Run 2 Spiked**

Min/Pt	Gas Sample	DGM Temp (°F)	Volume Metered Vrnstd (L)
5	Volume		
Elapsed Time	Initial (L)		
	0.00		
5	2.001	102	1.844
10	3.989	103	1.829
15	6.011	105	1.854
20	8.041	105	1.861
25	10.023	107	1.811
30	12.025	109	1.823
35	14.010	111	1.801
40	16.029	112	1.828
45	18.013	113	1.794
50	20.081	114	1.866
55	22.037	114	1.765
60	24.058	116	1.818
65	26.008	117	1.751
70	28.017	117	1.804
75	30.068	117	1.841
80	32.072	118	1.796
85	34.095	118	1.813
90	36.070	119	1.767

**Totals and Averages**

90	36.041	111	32.99
----	--------	-----	-------

**Totals and Averages**

90	36.070	112	32.66
----	--------	-----	-------

Project Number	3648
Client	Big Rivers
Plant	Henderson
Location	Stack
Date	8/4/11
P <sub>b</sub> (Inches Hg)	29.41

Meter ID	R20078
Y <sub>d</sub>	1.0072

Start Time	13:11
Stop Time	15:00

Meter ID	R20078
Y <sub>d</sub>	0.9985

**Run 3**

Min/Pt	Gas Sample	DGM	Volume
5	Volume	Temp	Metered
Elapsed	Initial (L)	(°F)	Vrnsid
Time	0.00		(L)
5	2.122	104	1 966
10	4.097	103	1 833
15	6.029	104	1 790
20	8.012	105	1 834
25	10.046	107	1 874
30	12.016	109	1 809
35	14.071	111	1 881
40	16.076	113	1 828
45	18.047	115	1 791
50	20.029	116	1 798
55	21.998	118	1 780
60	24.009	118	1 818
65	26.019	120	1 811
70	28.013	120	1 796
75	30.011	121	1 797
80	32.058	122	1 838
85	34.081	122	1 816
90	36.072	123	1 784

**Run 3 Spiked**

Min/Pt	Gas Sample	DGM	Volume
5	Volume	Temp	Metered
Elapsed	Initial (L)	(°F)	Vmstd
Time	0.00		(L)
5	2.012	103	1 851
10	4.054	103	1 879
15	6.022	104	1 808
20	8.044	106	1 851
25	10.024	109	1 803
30	12.032	111	1 822
35	14.029	114	1 802
40	16.025	116	1 795
45	18.054	117	1 822
50	20.019	118	1 761
55	22.081	120	1 842
60	24.087	120	1 792
65	26.073	121	1 771
70	28.047	122	1 757
75	30.042	122	1 776
80	32.061	123	1 794
85	34.067	123	1 782
90	36.084	124	1 789

**Totals and Averages**

90	36.072	114	32.84
----	--------	-----	-------

**Totals and Averages**

90	36.084	115	32.49
----	--------	-----	-------