Archived: Thursday, May 31, 2012 3:41:10 PM From: Eric M. Robeson Sent: Monday, December 12, 2011 6:01:40 PM To: ADAM.C.LANDRY@sargentlundy.com Subject: Re: SL-010881 Big Rivers Electric Corporation - Environmental Compliance Study (Final) Importance: Normal

Will not occur. Mgt wants to digest report first. Will be back in office tomorrow On Dec 12, 2011, at 5:47 PM, "ADAM.C.LANDRY@sargentlundy.com" <ADAM.C.LANDRY@sargentlundy.com> wrote: > > Eric - any feedback on an S&L presentation / meeting this Friday? > > > Best Regards. > Adam C. Landry PE > > > ----- Original Message -----> From: ADAM C LANDRY Sent: 12/09/2011 01:47 PM CST > To: eric.robeson@bigrivers.com > > Cc: TODD HANSSEN; CALEB KADERA > Subject: SL-010881 Big Rivers Electric Corporation - Environmental > Compliance Study (Final) > Eric, > Attached is the final report for the Environmental Compliance Study. If > you have any additional comments, we can quickly make those modifications > and reissue early next week. > (See attached file: SL-010881 Big Rivers Electric Corporation -> Environmental Compliance Study (Final).pdf) > > > > As a summary, below are the specific responses to the comments and > questions raised on the draft report: > > > Item 1: Section 1.1 - Not sure escalating gas price 2.5% per year is > correct. What does that give us 10/20 years out? > Response 1: A sensitivity analysis was conducted on our initial price > assumption and used to justify conclusions for natural gas modifications. > Report has been updated accordingly. > > Item 2: Section 3.2.1.1.2 - 3rd line talks about lime slurry; should > also reflect limestone slurry > Response 2: Report has been updated > Item 3: Section 3.2.1.2 - Comment section for Coleman FGD: We believe we

> operate much higher than 93.5% > Response 3: "return to design" condition reflects an emission rate of 0.25 > lb/MMBtu. These "reductions" are reflective of the differential between > the reported EPA data and the 0.25lb/MMBtu rate provided by BREC > Item 4: Section 3.2.4.1.1 - Don't' believe ESP upgrades will be adequate > at Coleman and HMPL (see comments #2 for more details > Response 4: Response included in detail further below in Response 16. > > Item 5: Section 3.2.6.1.4 - Last line paragraph 2 - We believe cooling > tower is an option at Coleman > Response 5: Paragraph adjusted to state that it is not economically > justifiable for 316(b) when compared to other available options. > > Item 6: Section 4.1.4 - One of only 5 still in existence? Thought Wilson > and Gibson were only ones still inexistence, and only 5 were ever built > Response 6: Kellogg Weir Scrubbers were built Thomas Hill 3 - Not in operation > > Gibson 5 - Being replaced Bruce Mansfield 3 - In Operation > Coronado Units 1 & 2 - Unit 2 has been replaced and Unit > > 1 replacement is in construction D B. Wilson - In Operation > > Item 7: Section 4.1.5 - Doesn't' really say what conclusion is i.e. > Wilson FGD, HMPL upgrade > Response 7: Section was removed > Item 8: Section 4.3.5 - Doesn't really say what conclusion is > Response 8: Section was removed > > Item 9: Section 4.4.2 - Coleman and HMPL issue: not adequate > Response 9: Report has been revised > > Item 10: Section 4.6.1 - Can Coleman really achieve this much improvement? > Response 10: See response to Item 3 above > > Item 11: Section 4.6.1 - Table 4-3 - typo Advanced Burners (hanging d) > Response 11: Report has been revised > > Item 12: Section 5.1.1 - Last 2 lines - pretty broad wiggle words +/-> 20% in section 1.1.1 > Response 12: Report has been revised > > Item 13: Section 5.2.1 - Paragraph under Table 5-5: last sentence > natural gas conversion ... "does not appear to be economically justifiable" > ..... > Response 13: Report has been revised > Item 14: Section 5.2.2 - Table 5-6 - Where did NPV numbers come from? > What is NPV for various SO2, NOx, MACT options? How were they calculated? > (do we need these type of tables in another appendix, or in body of report > somewhere?) > Response 14: Calculation tables have been added to appendix > Item 15: Section 5.3.1 - Figure 5-4 and Table 5-8: talked to Caleb about > this: signs seem backward: surplus should be positive number (at first > glance I thought I was really short SO2 in early years) > Response 15: Introductory statement and figure headings have been revised > to indicated that the plot represents cumulative emissions above or below > allocations. The "O" line represents BREC emitting exactly their allowance

## > tonnage.

>

> Item 16: Precipitator Upgrades: I do not believe that ESP upgrades will > work at Coleman or HMP&L. The precipitators on these units are quite small > compared to Green and Wilson having only three collecting fields compared > to seven or more for the other units. The physical sizes of the > precipitator boxes are quite small, and the gas velocity through the > collecting fields is more than double what is recommended for effective > particle collection. Without increasing the physical size of the boxes > enough to reduce the gas velocity to allow sufficient time for particle > charging I don't believe PM collection will improve. If we use ACI at > Coleman for Mercury control I know that it takes significantly longer to > charge the carbon particles than to charge fly ash for collection. We > learned that while experimenting with burning pet coke in the HMP&L units. > I don't know what the resistivity is for hydrated lime if we choose it for > SO3 control at HMP&L, but if it is greater than fly ash, I expect that it > will pass through the precipitator to the WFGD. > Response 16: The testing that BREC performed at the Coleman and HMP&L > systems showed that the PM emissions were above the proposed MACT limits > primarily due to condensible PM emissions as can be seen in the table > below. > (Embedded image moved to file: pic19169.gif) > The recommended use of dry sorbent (hydrated lime) injection to reduce the > condensible PM emissions with only a slight increase in inlet dust loading > to the ESP. S&L is working with another Utility client to upgrade their > older, existing, ESPs. The upgrade plans involve replacement of the > discharge electrodes (DE) with newer advanced designs with more discharge > points and also replacement of the existing T/R sets with high frequency > T/R sets permitting more power to charge the fly ash in the ESP. Coupled > with replacement of the conventional T/R sets will be some increased > sectionalization of the existing precipitators for both power (less plate > area be "served" by a single T/R set) and reliability reasons (loss of a > T/R set has less of an effect on overall ESP performance). These upgrades > are on ESP's that are over 30 years old which are the same age range as the > ESP's at HMP&L and Coleman. > Additionally, S&L has recently participated in a number of activated carbon > injection tests where PM was measured both baseline and during the tests. > With carbon injection rates as high as 9 lb activated carbon/million acf > there was minimal increases in the outlet PM loading. Testing with > hydrated lime has also shown minimal increases in the particulate loading. > As was pointed out by BREC, any lime that penetrates the ESP will pass > through to the wet FGD systems at HMP&L and Coleman and will aid in SO2 > removal. Under the proposed Utility MACT particulate monitoring will be > performed in the chimney (as is done now by the PM monitors operating at > HMP&L 1 & 2). Report has been updated. > > Item 17: Reid/HMP&L Fly Ash Collection - Just a reminder that the fly ash > transport system from the dry ash collectors to the HMP&L storage silo is > also pressure pneumatic. I did not notice that mentioned in table 2-8. > Response 17: Report has been revised > > Item 18: Sebree Intake Structure 316(b) Compliance - If the Reid 1 Unit is > retired the Circulating Water Pumps at the intake structure could be > downsized for make up to the HMP&L cooling towers, HMP&L units sluice water

> make up, and to supply HWU's South Water Treatment facility. As stated in
> the paragraph following Table 4.4 on page 4-13, a study would need to be

> conducted to determine the pump size required, and if the reduced

> requirement would bring the overall intake flow velocity below the 0.5 fps > limit.

> Response 18: Report has been revised

>

> Item 19: Reid/HMP&L Waste Water Streams - The entire Reid/HMP&L plant foot > print drains to a sump adjacent to the HMP&L fly ash silo and is pumped to > the ash pond for disposal. As mentioned in the last paragraph on page 4-14 > a waste water treatment facility would need to be added or the site sump > redirected to the Green Station waste water treatment facility before the > existing ash pond could be closed. > Response 19: Report has been revised > > Item 20: Page 2-10 Table 2-8 - Wilson Pyrites Handling "Sluiced to Bottom > Ash SSC"should read "Handled Dry"; Modifications Required "Eliminate Ash > Storage Ponds and install Dewatering Equipment" should read "Dewatering > Equipment in Place, Ash Handled Dry" > Response 20: Report has been revised > Item 21: Page 3-4 Table 3-1 Wilson Increase L/G - This is the premise for > URS proposed modifications for Kellogg scrubbers; however, field experience > at other utilities does not support their theoretical removal rates; > therefore I question the validity of offering this as a viable control > strategy. Past experimentation leads me to believe that changes in L/G do > not produce results of the anticipated magnitude primarily due to inherent > inefficiencies in the cross current design. Additives - "Either DBA or > Sodium Formate could be used" .... should read "Currently using both DBA and > Sodium Bisulfite .....' > Response 21: Report has been revised > Item 22: Page 3-18 Section 3.2.7.2 CCR Strategies - Wilson Station does > not have an ash pond. > Response 21: Report has been revised > Item 23: Page 4-3 Section 4.1.3 Additives - "In the past, this organic > acid ....." should read "Wilson Station currently uses organic acid to > enhance FGD performance." > Response 21: Report has been revised > > Item 24: Page 4-8 Section 4.4.3 Sorbent Injection - Wilson Station > currently has a DSI system, are we already obtaining some amount of CPM > reduction? If so is the estimated 50% reduction realistic? - report has > been revised to indicate > Response 24: Wilson has a DSI system in place accounts for slight > improvement in reduction with increased hydrated lime injection. 50% > reduction can be expected for Coleman and HMP&L. (see Response 16) > > > > Regards, > > Adam C. Landrv > Professional Engineer of Indiana, Illinois, Alberta > Project Manager > Sargent & Lundy, LLC > 55 East Monroe Street > Chicago, Illinois 60603 > Phone: 312-269-7292 > Cell: 312-656-2464 > Fax: 312-269-9602 > <SL-010881 Big Rivers Electric Corporation - Environmental Compliance Study (Final).pdf> > <pic19169.gif>